## **AMENDMENTS TO THE CLAIMS**

This listing of claims will replace all prior versions and listings of claims in the application:

## LISTING OF CLAIMS:

(currently amended): A fluoropolymer producing method
 which comprises polymerizing a radical polymerizable monomer in a manner of
 continuous polymerization in a defined reaction-field to give the fluoropolymer,

wherein said defined reaction-field is in a supercriticality-expression state and under a pressure of not higher than 40 MPa and a temperature of not higher than that higher by 100°C than the supercriticality-expression temperature of the defined reaction-field,

said radical polymerizable monomer comprises a fluorine-containing ethylenic monomer, and

said fluoropolymer has a weight average molecular weight [Mw] of not lower than 150,000 as determined on the polystyrene equivalent basis and

a ratio [Mw/Mn] of the weight average molecular weight [Mw] on the polystyrene equivalent basis to a number average molecular weight [Mn] of the fluoropolymer on the polystyrene equivalent basis is higher than 1 but not higher than 3, substantially without using an aqueous medium.

2. (currently amended): A fluoropolymer producing method

which comprises polymerizing a radical polymerizable monomer in a manner of continuous polymerization in a defined reaction-field in the presence of carbon dioxide to give the fluoropolymer,

wherein said defined reaction-field is in a supercriticality-expression state,
said radical polymerizable monomer comprises a fluorine-containing ethylenic monomer,
said carbon dioxide amounts to at most equimolar to said radical polymerizable
monomer, and

said fluoropolymer has a weight average molecular weight [Mw] of not lower than 150,000 as determined on the polystyrene equivalent basis and

a ratio [Mw/Mn] of the weight average molecular weight [Mw] on the polystyrene equivalent basis to a number average molecular weight [Mn] of the fluoropolymer on the polystyrene equivalent basis is higher than 1 but not higher than 3, substantially without using an aqueous medium.

- 3. (original): The fluoropolymer producing method according to claim 2, wherein said defined reaction-field further is under a pressure of not higher than 40 MPa and a temperature of not higher than that higher by 100°C than the supercriticality-expression temperature of said defined reaction-field.
- 4. (previously presented): The fluoropolymer producing method according to claim 1 or 2,

wherein said defined reaction-field has a ratio  $[\rho_m/\rho_0]$  of not lower than 1.1, the ratio  $[\rho_m/\rho_0]$  is of a monomer density  $[\rho_m]$  of a monomer critical density  $[\rho_0]$ .

5. (previously presented): The fluoropolymer producing method according to claim1,

wherein the polymerization of the radical polymerizable monomer is carried out in the presence of a chain transfer agent.

- 6. (original): The fluoropolymer producing method according to claim 5, wherein the continuous polymerization is carried in a condition that an amount of the fluoropolymer in a reaction vessel amounts to at least 8 g per liter of the capacity of said reaction vessel in a steady state.
- 7. (previously presented): The fluoropolymer producing method according to claim 1 or 2,

wherein the fluorine-containing ethylenic monomer comprises at least one species selected from the group consisting of vinylidene fluoride, tetrafluoroethylene, chlorotrifluoroethylene and hexafluoropropylene.

8. (previously presented): The fluoropolymer producing method according to claim 1 or 2,

wherein the fluorine-containing ethylenic monomer comprises vinylidene fluoride.

9. (previously presented): The fluoropolymer producing method according to claim 1,

wherein the polymerization of the radical polymerizable monomer is carried out in the presence of a radical polymerization initiator.

10. (original): The fluoropolymer producing method according to claim 9,

wherein the radical polymerization initiator is an organic peroxide.

- 11. (original): The fluoropolymer producing method according to claim 10, wherein the organic peroxide comprises a peroxydicarbonate, a fluorine-based diacyl peroxide and/or a fluorine-free diacyl peroxide.
- 12. (previously presented): The fluoropolymer producing method according to claim 1 or 2,

wherein the polymerization of the radical polymerizable monomer is carried out in the presence of a nonethylenic fluorocarbon.

- 13. (previously presented): The fluoropolymer producing method according to claim 2, wherein the polymerization of the radical polymerizable monomer is carried out in the presence of a chain transfer agent.
- 14. (previously presented): The fluoropolymer producing method according to claim 13, wherein the continuous polymerization is carried in a condition that an amount of the fluoropolymer in a reaction vessel amounts to at least 8 g per liter of the capacity of said reaction vessel in a steady state.
- 15. (previously presented): The fluoropolymer producing method according to claim 2, wherein the polymerization of the radical polymerizable monomer is carried out in the presence of a radical polymerization initiator.
- 16. (previously presented): The fluoropolymer producing method according to claim 15, wherein the radical polymerization initiator is an organic peroxide.

- 17. (previously presented): The fluoropolymer producing method according to claim 16, wherein the organic peroxide comprises a peroxydicarbonate, a fluorine-based diacyl peroxide and/or a fluorine-free diacyl peroxide.
- 18. (previously presented): The fluoropolymer producing method according to claim 1, which comprises continuously supplying the radical polymerizable monomer to the defined reaction-field and continuously discharging fluoropolymer product from the reaction-field.
- 19. (previously presented): The fluoropolymer producing method according to claim 2, which comprises continuously supplying the radical polymerizable monomer to the defined reaction-field and continuously discharging fluoropolymer product from the reaction-field.